

Carbon Balance

This notebook contains calculations to estimate carbon balances on the reactors

Import data from web page

Read the Exp1.dat file. Drop the first two records that correspond to TecPlot header

```
In[20]:= exp1Dat = Import["http://dryas.mbl.edu/A2M/Exp1/data/Exp1.dat"][[3 ;;]]
```

```
Out[20]= {{5, 21, 2015, 19, 52, 51, 20.9, 0.02, 0.23, 0.05, 0, 0.0144, 0.1542,  
0.81972, 1, 3, 4.2, 227, 20, 20.75, 0.03, -0.0036, 7.389, 280.84,  
0.82831, 2, 15.5, 7, 229.4, 19.9, 18.21, 0.014, 0.0964, 7.325, 272.46, 0},  
... 1740 ..., {10., 18., 2015., 9., 58., 4., 20.48, 2.08, -0.54, 0.027,  
0.061, 0.0136, 0.1276, 150.406, ... 8 ..., 7.024, 320.86, 150.415,  
2., 17.9, 4.6, 231.1, 29.9, 0.56, 0.263, 0.3388, 7.359, 5.04, 0}}}
```

large output

show less

show more

show all

set size limit...

The dimension of the data array is:

```
In[21]:= Dimensions[exp1Dat]
```

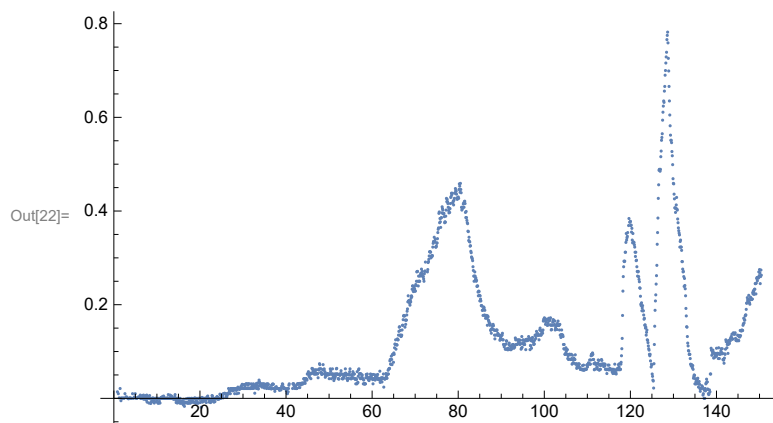
```
Out[21]= {1742, 36}
```

Digester Carbon Balance

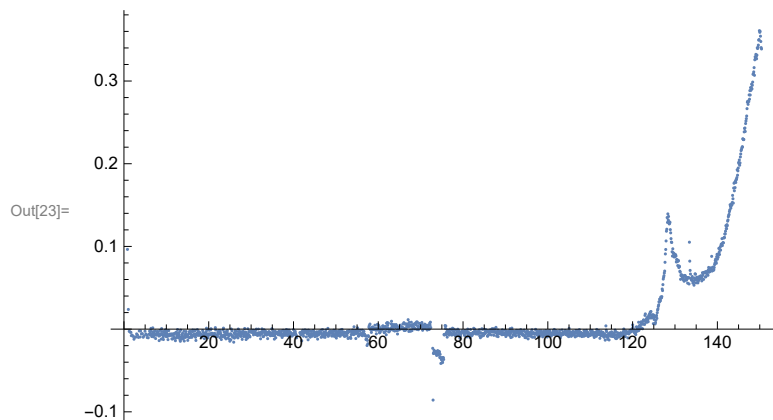
Some crude estimates of carbon export from the digester are calculated in this section. Note, these simple calculations do not account for C exchange between the reactors when the exchange pump is on. There is a very large carbon import from the algal reactor via carbonate chemistry that needs to be accounted for.

Below are plots of CO₂, CH₄ (in %) and gas flow rate (mL/min) to digester since this notebook was last executed.

```
In[22]:= ListPlot[exp1Dat[[All, {25, 32}]], PlotRange -> All]
```

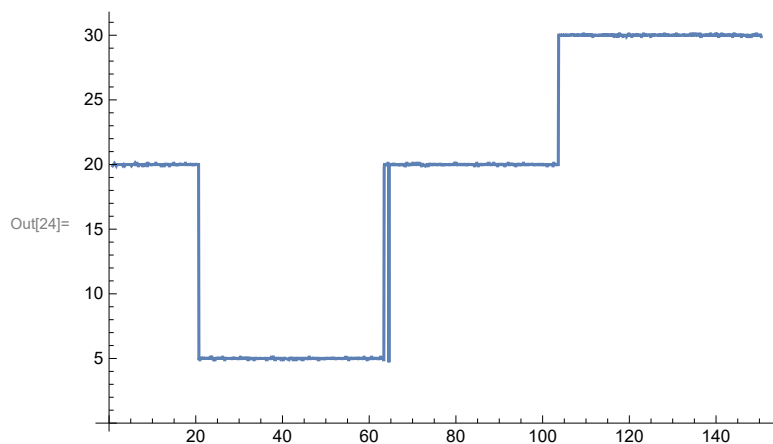


```
In[23]:= ListPlot[exp1Dat[[All, {25, 33}]], PlotRange -> All]
```



Gas flow rate to digestor (in mL/min) is given here:

```
In[24]:= ListLinePlot[exp1Dat[[All, {25, 30}]]]
```



Fit interpolating polynomials to CO₂ and CH₄ data.

```
In[25]:= co2Digestor = Interpolation[exp1Dat[[2 ;;]]][All, {25, 32}]]
```

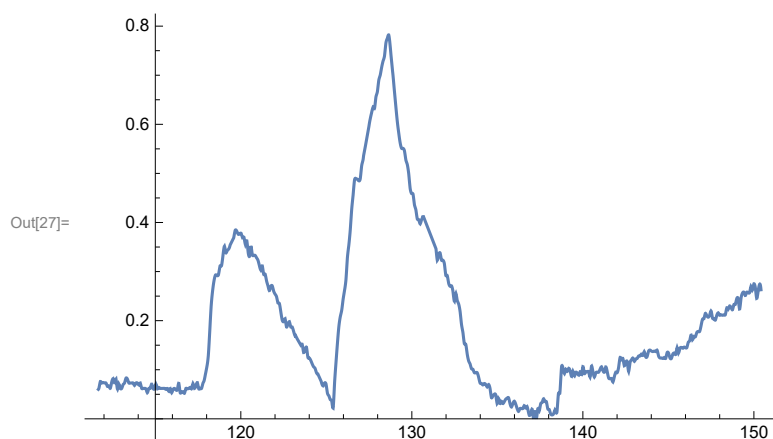
```
Out[25]= InterpolatingFunction[  Domain: {{1.04, 150.}}  
Output: scalar]
```

```
In[26]:= ch4Digestor = Interpolation[exp1Dat[[2 ;;]]][All, {25, 33}]]
```

```
Out[26]= InterpolatingFunction[  Domain: {{1.04, 150.}}  
Output: scalar]
```

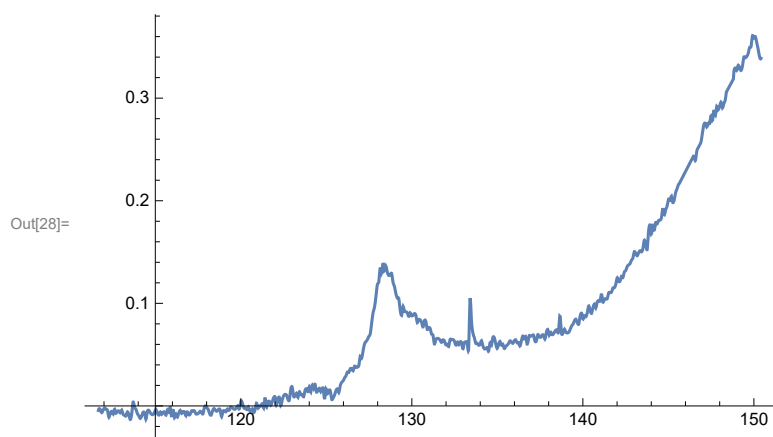
CO₂ leaving the reactor:

```
In[27]:= Plot[co2Digestor[t], {t, 111.67, Last[exp1Dat][[25]]}]
```



Methane leaving digester:

```
In[28]:= Plot[ch4Digestor[t], {t, 111.67, Last[exp1Dat][[25]]}]
```



The number of mmols of CO₂ or CH₄ produced right after the addition of acetate and glucose is calculated from the ideal gas law ($n = PV/RT$) where volume is given by the flow rate (flow rate was 30 mL/min or 43.2 L/d) and the partial pressure of CO₂ or CH₄ is determined by integrating over the time interval of interest. Since flow rate was constant, it can be pulled out of the integral, but if it changes then it needs to be left in.

For CO₂, the total carbon leaving the digester is given by

```
In[29]:= 
$$\frac{1000}{100} \left( \frac{43.2}{298 \times 0.082057} \right) \left( \int_{111.67}^{\text{Last}[\text{exp1Dat}][[25]]} \text{co2Digester}[t] \, dt \right) \text{ " (mmol CO}_2\text{) "}$$

Out[29]= 133.71 (mmol CO2)
```

However, this calculation does not account for the significant amounts of DIC (dissolved inorganic carbon) entering the reactor from the algal reactor via the carbonate system. Consequently, the above value is of not much meaning with regard to glucose or acetate consumed. Instead look at methane output, which is given by,

```
In[30]:= 
$$\text{ch4Totalmmol} = \frac{1000}{100} \left( \frac{43.2}{298 \times 0.082057} \right) \left( \int_{111.67}^{\text{Last}[\text{exp1Dat}][[25]]} \text{ch4Digester}[t] \, dt \right) \text{ " (mmol CH}_4\text{) "}$$

Out[30]= 56.9673 (mmol CH4)
```

One mM of glucose was added to the 18 L digester, which could have produced a maximum (under aerobic conditions) of 108 mmol CO₂, while the 1 mM of acetate would produce 36 mmol, so a total of 144 mmol. But, we need to account for dilution of glucose and Ac by exchange with algal reactor for the short time they were coupled (assume no glucose or Ac are consumed in the algal reactor). We also assume no labile carbon existed in the algal reactor during the exchange (a poor assumption). Based on the reactor volumes, the dilution factor would be $\frac{18}{18+4} = 0.818$, so this would mean there could have been 117.8 mmol of C.

Assuming a 50/50 ratio of CH₄ to CO₂ production, then the % consumed glucose and Ac in the digester is crudely approximated by twice the CH₄ production, or

```
In[31]:= {2 
$$\frac{\text{ch4Totalmmol}[[1]]}{117.8} 100 \text{ " \% at time " , Last}[\text{exp1Dat}][[25]]\}$$

Out[31]= {96.7186 % at time , 150.415}
```

The instantaneous CH₄ production rate (mmol/d) at the last sample point is given by:

```
In[32]:= 
$$\frac{\text{ch4Digester}[\text{Last}[\text{exp1Dat}][[25]]]}{100} 1000 \left( \frac{60 \times 24 \text{ Last}[\text{exp1Dat}][[30]] / 1000}{298 \times 0.082057} \right) \text{ " (mmol/d) "}$$

Out[32]= 5.96548 (mmol/d)
```